

IN THE CLAIMS

Please amend the claims as follows:

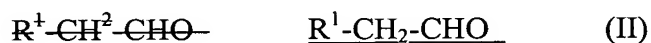
Claims 1-17 (Canceled)

18. (Currently Amended) A process for the production of an alkyl-substituted butenol having the formula (I):



wherein  $R^1$  is a saturated or olefinically unsaturated alkyl or cycloalkyl group having from 4 to 16 carbon atoms and wherein  $R^1$  is optionally substituted by an alkyl, cycloalkyl, aryl or alkaryl having up to 12 carbon atoms; and  $R^2$  is hydrogen or an alkyl group having from 1 to about 6 carbon atoms the process comprising:

by reacting at least one aldehyde of the formula (II) with at least one corresponding lower aldehyde:



and  $R^1$  has the same meaning as in formula (I);

wherein:

- (i) aldol condensation is carried out in an inert organic solvent, and
- (ii) reduction of the unsaturated aldehydes is carried out in the presence of an optionally calcined copper/zinc catalyst, and is carried out continuously under isothermal conditions at a temperature ranging from 45 to 60°C and under a hydrogen pressure of 1 to 300 bar at an LHSV (liquid hourly space velocity) of 0.3 to 3.0 hr<sup>-1</sup>.

19. (Previously Presented) The process of claim 18, wherein the aldol condensation is carried out in a nonpolar organic solvent which can form an azeotrope with water.

20. (Previously Presented) The process of claim 18, wherein the aldol condensation is carried out in the presence of a catalyst which is an ammonium salt of an organic acid.

21. (Previously Presented) The process of claim 18, wherein  $R^2$  in formula (I) is a methyl group.

22. (Previously Presented) The process of claim 18, wherein  $R^2$  in formula (I) is a methyl group and wherein propionaldehyde is used in a 2.5 to 10-fold molar excess based on the aldehyde of formula (II).

23. (Previously Presented) The process of claim 22, wherein the propionaldehyde is used in a 2.5 to 3.5-fold molar excess based on the aldehyde of formula (II).

24. (Previously Presented) The process of claim 18 wherein  $R'$  is a 4-(2,2,3-trimethylcyclopent-3-en-1-yl) group.

25. (Previously Presented) The process of claim 18, wherein the organic solvent in (i) is selected from the group consisting of toluene, xylene, benzene, cyclohexane and methyl cyclohexane.

26. (Previously Presented) The process of claim 18, wherein  $R^1$  is a saturated alkyl group having from 4 to 16 carbon atoms.

27. (Previously Presented) The process of claim 18, wherein  $R^1$  is an olefinically unsaturated alkyl group having from 4 to 16 carbon atoms.

28. (Previously Presented) The process of claim 18, wherein  $R^1$  is an olefinically unsaturated cycloalkyl group having from 4 to 16 carbon atoms.

29. (Previously Presented) The process of claim 18, wherein  $R^1$  is not further substituted.

30. (Previously Presented) The process of claim 18, wherein  $R^1$  is substituted by an alkyl, cycloalkyl, aryl or alkaryl having up to 12 carbon atoms.

31. (Currently Amended) The process of claim 18, wherein  $R^2$  is hydrogen.

32. (Currently Amended) The process of claim 18, wherein  $R^2$  is an alkyl group having from 2 to 6 carbon atoms.

33. (Previously Presented) The process of claim 18, wherein said LHSV (liquid hourly space velocity) ranges from 0.6 to 1.2  $\text{hr}^{-1}$ .

34. (New) A process for the production of an alkyl-substituted butenol having the formula (I):



wherein  $R^1$  is a saturated or olefinically unsaturated alkyl or cycloalkyl group having from 4 to 16 carbon atoms and wherein  $R^1$  is optionally substituted by an alkyl, cycloalkyl, aryl or alkaryl having up to 12 carbon atoms; and  $R^2$  is hydrogen or an alkyl group having from 1 to about 6 carbon atoms the process comprising:

by reacting at least one aldehyde of the formula (II) with at least one corresponding lower aldehyde:



and  $R^1$  has the same meaning as in formula (I);

wherein:

- (i) aldol condensation is carried out in an inert organic solvent, and
  - (ii) reduction of the unsaturated aldehydes is carried out in the presence of an optionally calcined copper/zinc catalyst, and
- is carried out continuously in a fixed bed reactor at a LHSV (liquid hourly space velocity) of 0.3 to 3.0 hr<sup>-1</sup>,
- under isothermal conditions at a temperature ranging from 45 to 60°C, and
- under a hydrogen pressure of 1 to 300 bar.